



US009309129B1

(12) **United States Patent**  
**Zeitoun et al.**

(10) **Patent No.:** **US 9,309,129 B1**  
(45) **Date of Patent:** **Apr. 12, 2016**

(54) **MULTI-EFFECTS DESALINATION SYSTEM**

(71) Applicant: **KING SAUD UNIVERSITY**, Riyadh (SA)

(72) Inventors: **Obida Mohamed Zeitoun**, Riyadh (SA); **Hany Abdelrahman Alansary**, Riyadh (SA); **Abdullah Othman Nuhait**, Riyadh (SA)

(73) Assignee: **KING SAUD UNIVERSITY**, Riyadh (SA)

(\*) Notice: Subject to any disclaimer, the term of this patent is extended or adjusted under 35 U.S.C. 154(b) by 0 days.

(21) Appl. No.: **14/667,626**

(22) Filed: **Mar. 24, 2015**

(51) **Int. Cl.**  
**B01D 1/26** (2006.01)  
**C02F 1/04** (2006.01)  
**B01D 1/28** (2006.01)  
**C02F 103/08** (2006.01)

(52) **U.S. Cl.**  
CPC ... **C02F 1/04** (2013.01); **B01D 1/26** (2013.01);  
**B01D 1/28** (2013.01); **C02F 2103/08** (2013.01)

(58) **Field of Classification Search**  
CPC ..... **C02F 1/04**; **C02F 2103/08**; **B01D 1/26**;  
**B01D 1/28**  
See application file for complete search history.

(56) **References Cited**

**U.S. PATENT DOCUMENTS**

3,351,120 A \* 11/1967 Goeldner et al. .... 159/13.3  
3,713,989 A \* 1/1973 Bom ..... 202/173  
3,844,899 A \* 10/1974 Sager, Jr. .... 202/173  
3,941,663 A \* 3/1976 Steinbruchel ..... 202/174

4,046,637 A \* 9/1977 Sasaki ..... 202/174  
4,330,373 A \* 5/1982 Liu ..... 202/174  
4,376,679 A \* 3/1983 Liu ..... 203/71  
5,139,620 A \* 8/1992 Elmore et al. .... 203/11  
7,799,178 B2 9/2010 Eddington  
7,922,874 B2 4/2011 Ophir et al.  
9,028,653 B2 \* 5/2015 Kwak et al. .... 202/174  
2010/0078306 A1 \* 4/2010 Alhazmy ..... 203/10  
2014/0263081 A1 \* 9/2014 Thiers ..... 210/718

**FOREIGN PATENT DOCUMENTS**

CN 101475231 A 7/2009  
CN 202016925 U 10/2011  
CN 102502903 A 6/2012  
CN 102992532 A 3/2013  
CN 102557168 B 10/2013  
WO WO 2005/100252 A1 10/2005

\* cited by examiner

*Primary Examiner* — Renee E Robinson

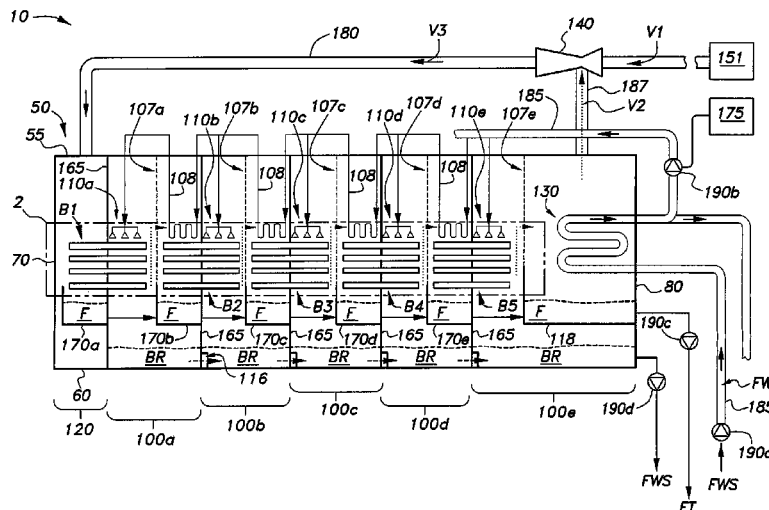
*Assistant Examiner* — Jonathan Miller

(74) *Attorney, Agent, or Firm* — Richard C. Litman

(57) **ABSTRACT**

A multi-effects desalination system includes a housing having a heating box, a plurality of vessels, a plurality of heat rods within each of the vessels, and a condenser unit. Each vessel is separated by a separator wall. Each heat rod extends through one of the separator walls, such that each heat rod has a first end extending into one vessel and a second end extending into an adjacent vessel. The desalination system also includes a plurality of sprayers, a plurality of demisters, and a plurality of trays. Each sprayer is configured to discharge feed water FW onto the second end of each heat rod in a respective vessel and each tray being configured to collect condensate or fresh water. The condensate collected in one to tray can be transferred to the condensate collection tray in an adjacent vessel. Further, the desalination system can also include a thermocompressor unit.

**7 Claims, 11 Drawing Sheets**



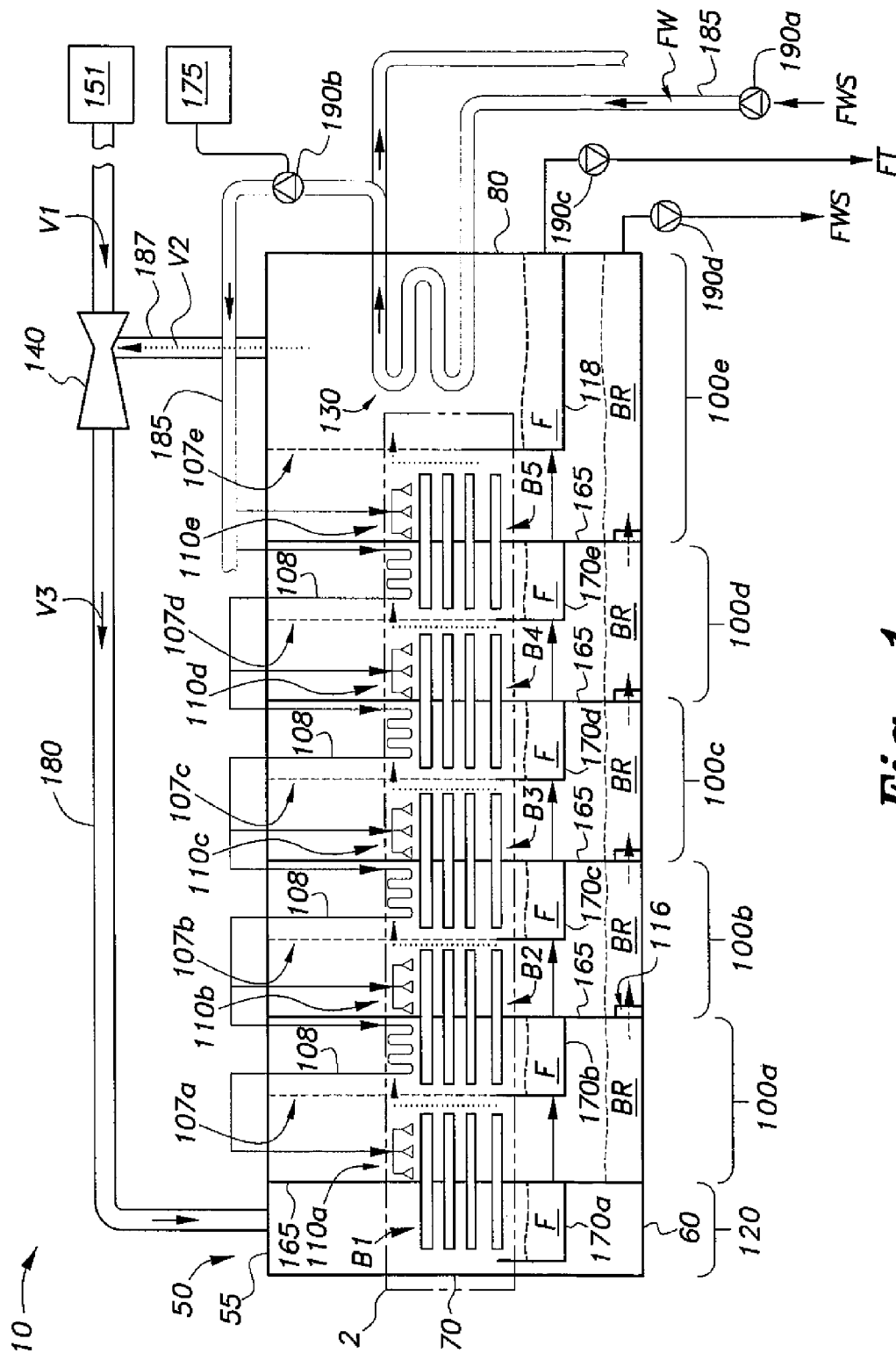
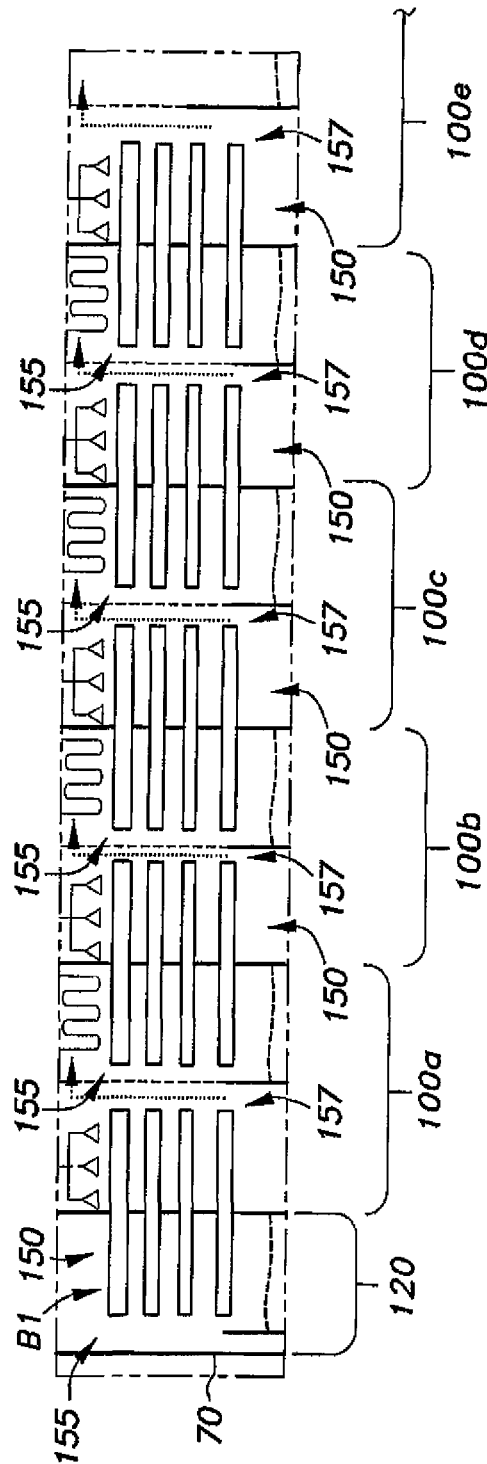
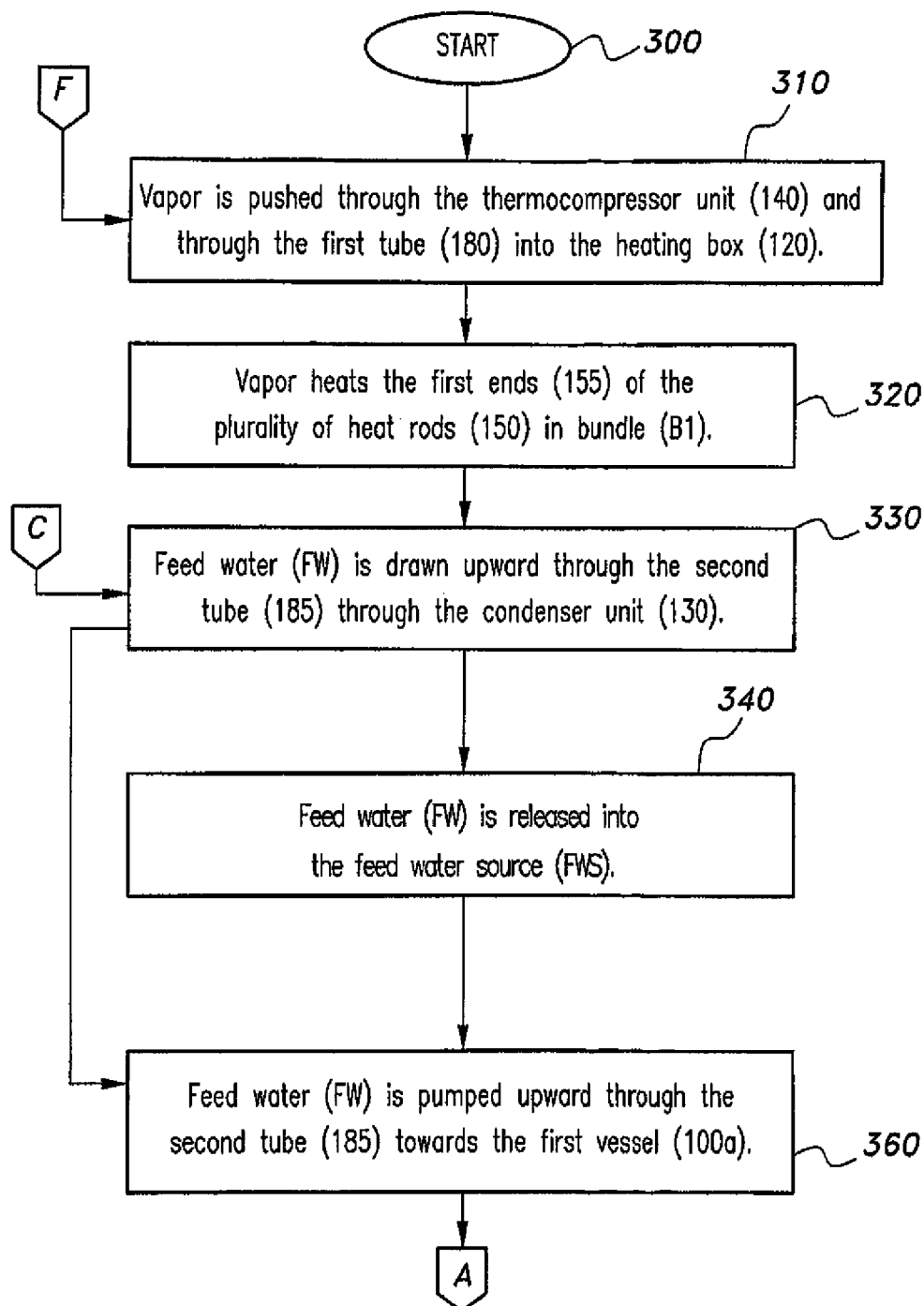
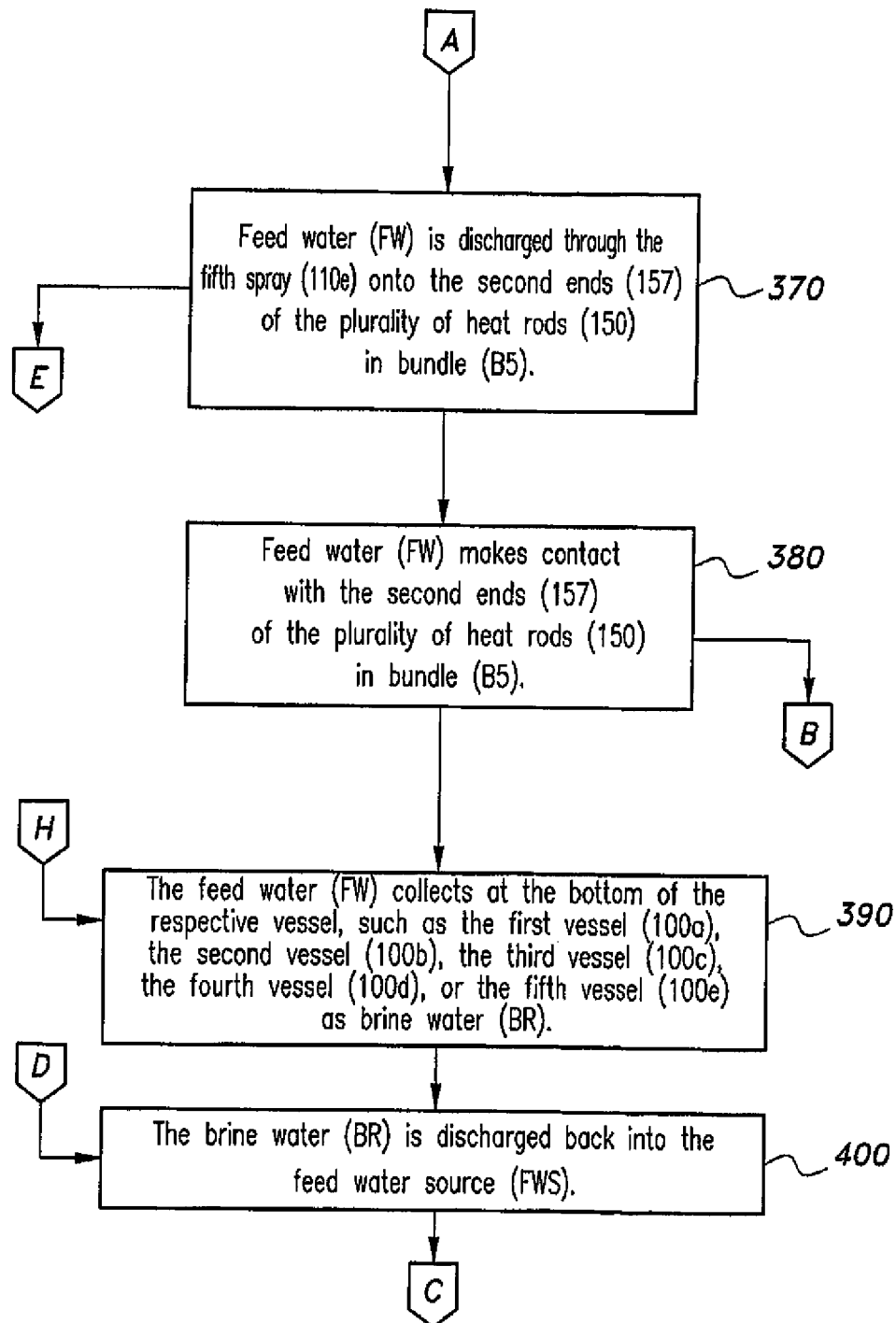


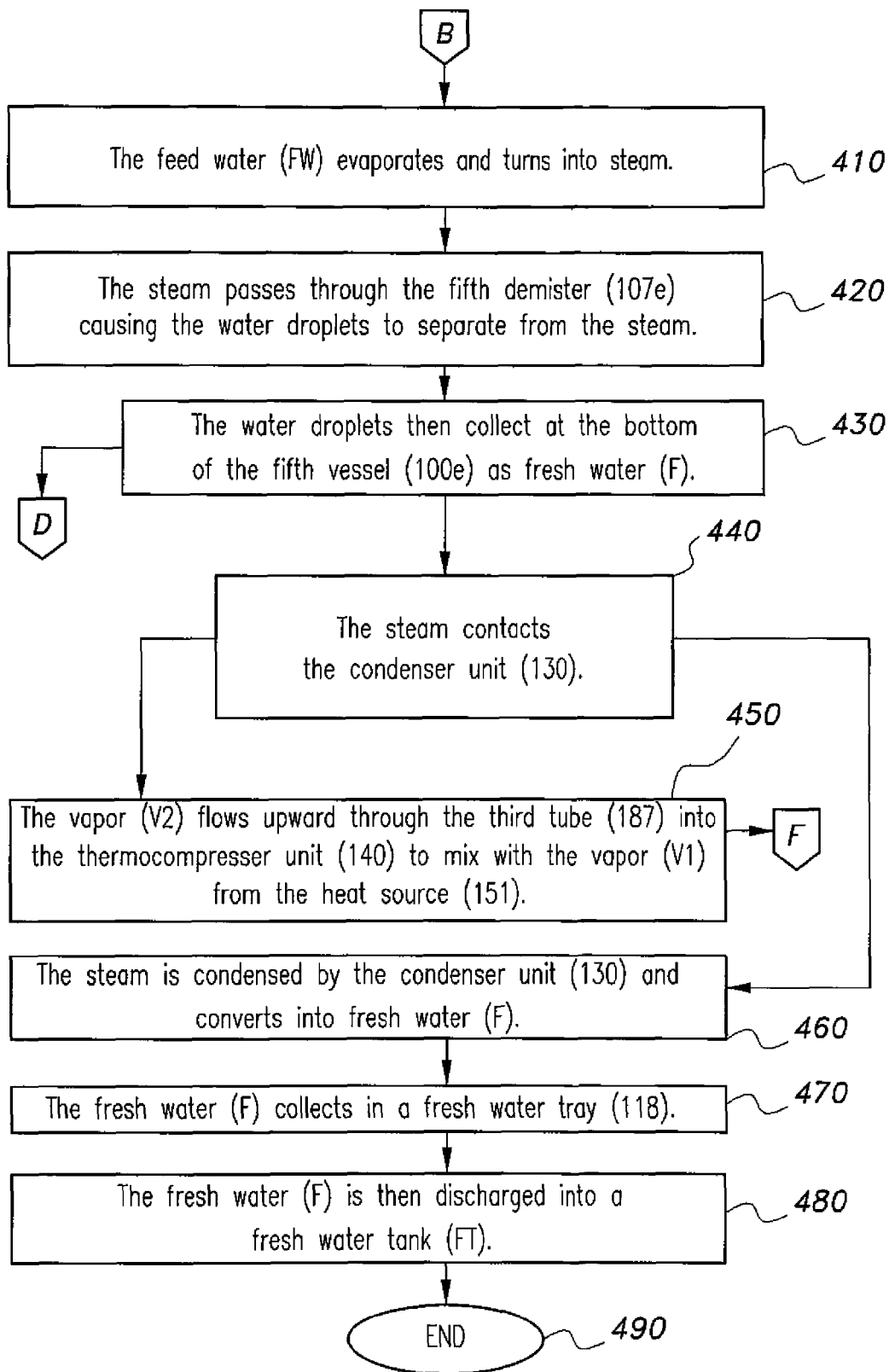
Fig. 1

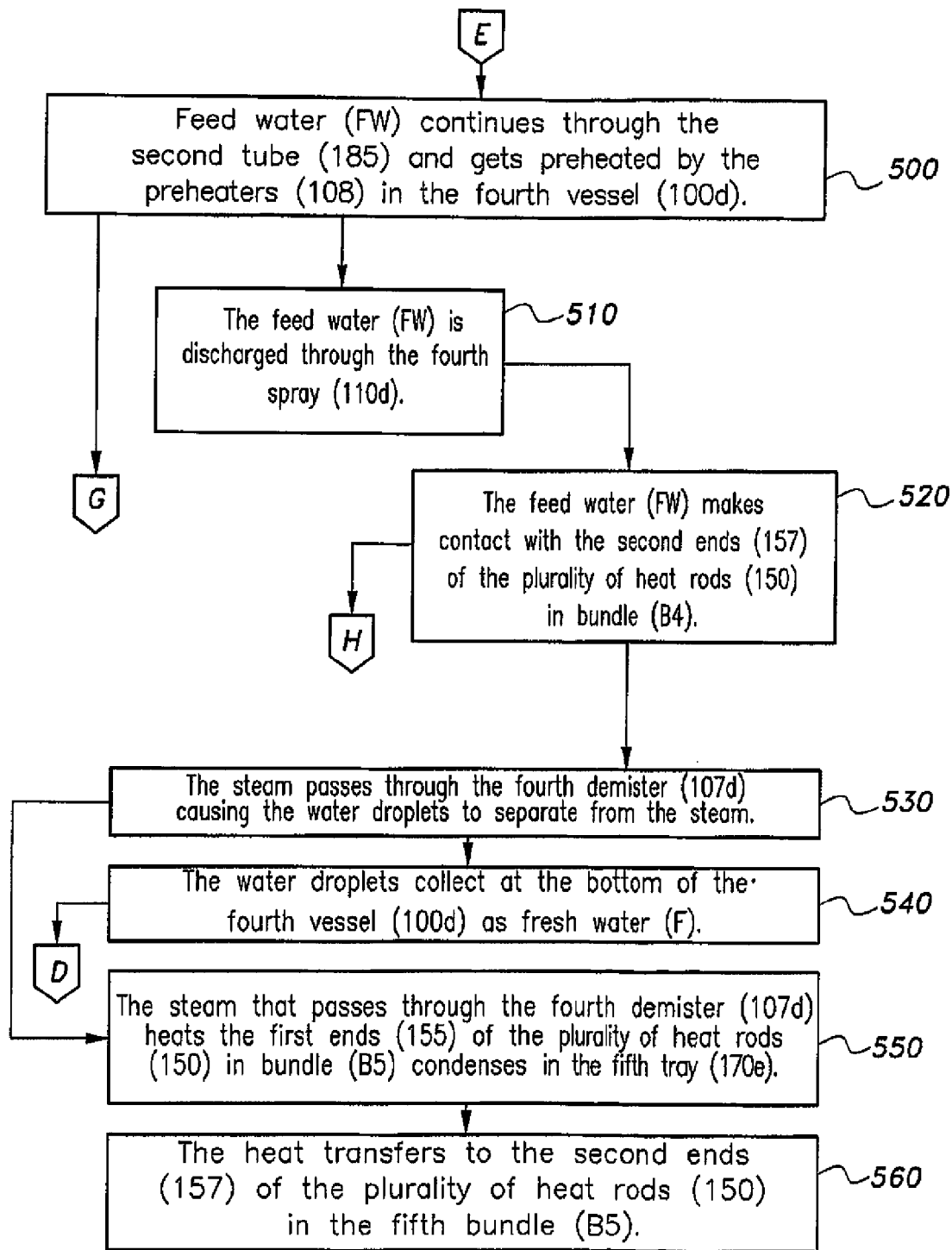


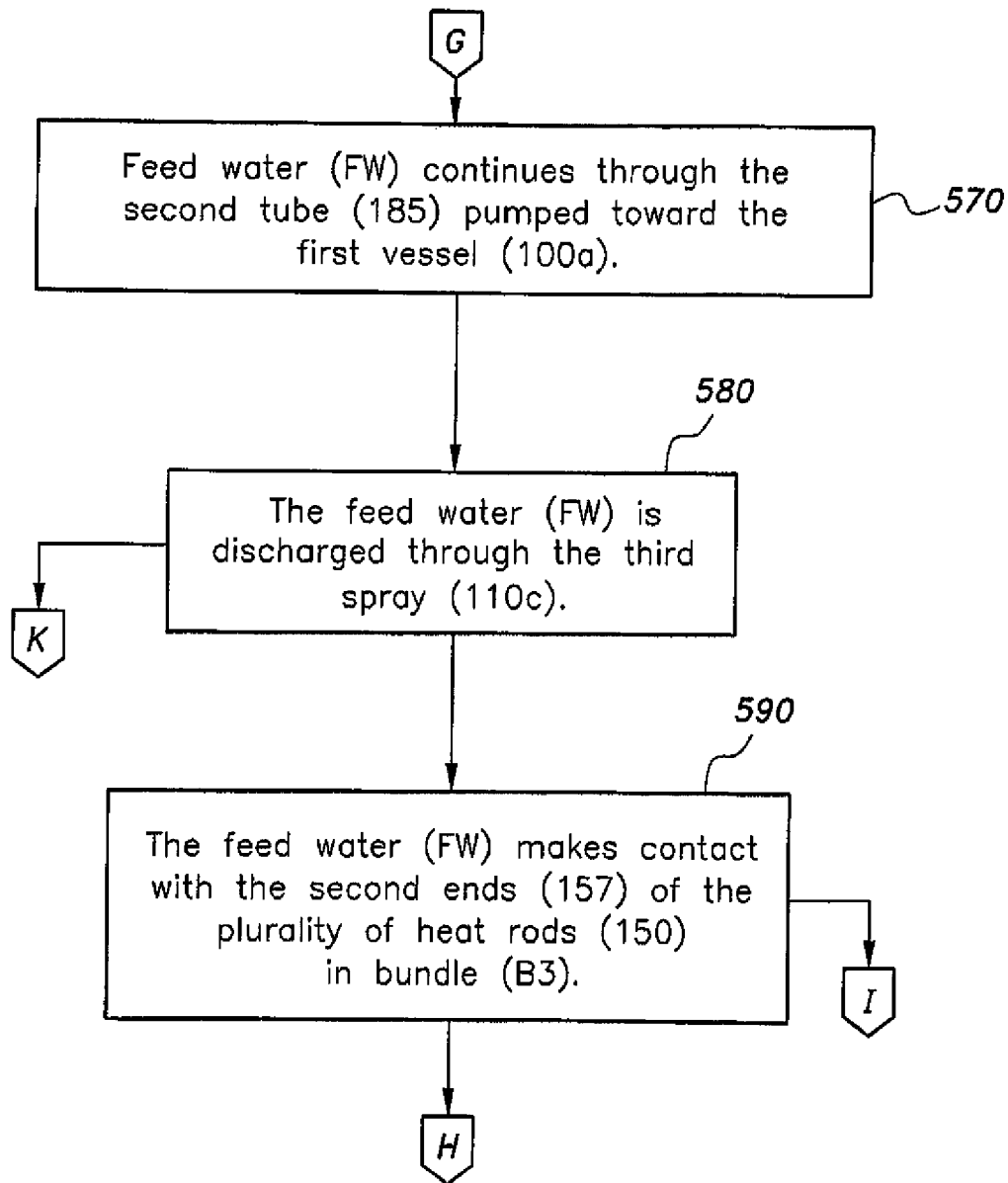
*Fig. 2*

*Fig. 3A*

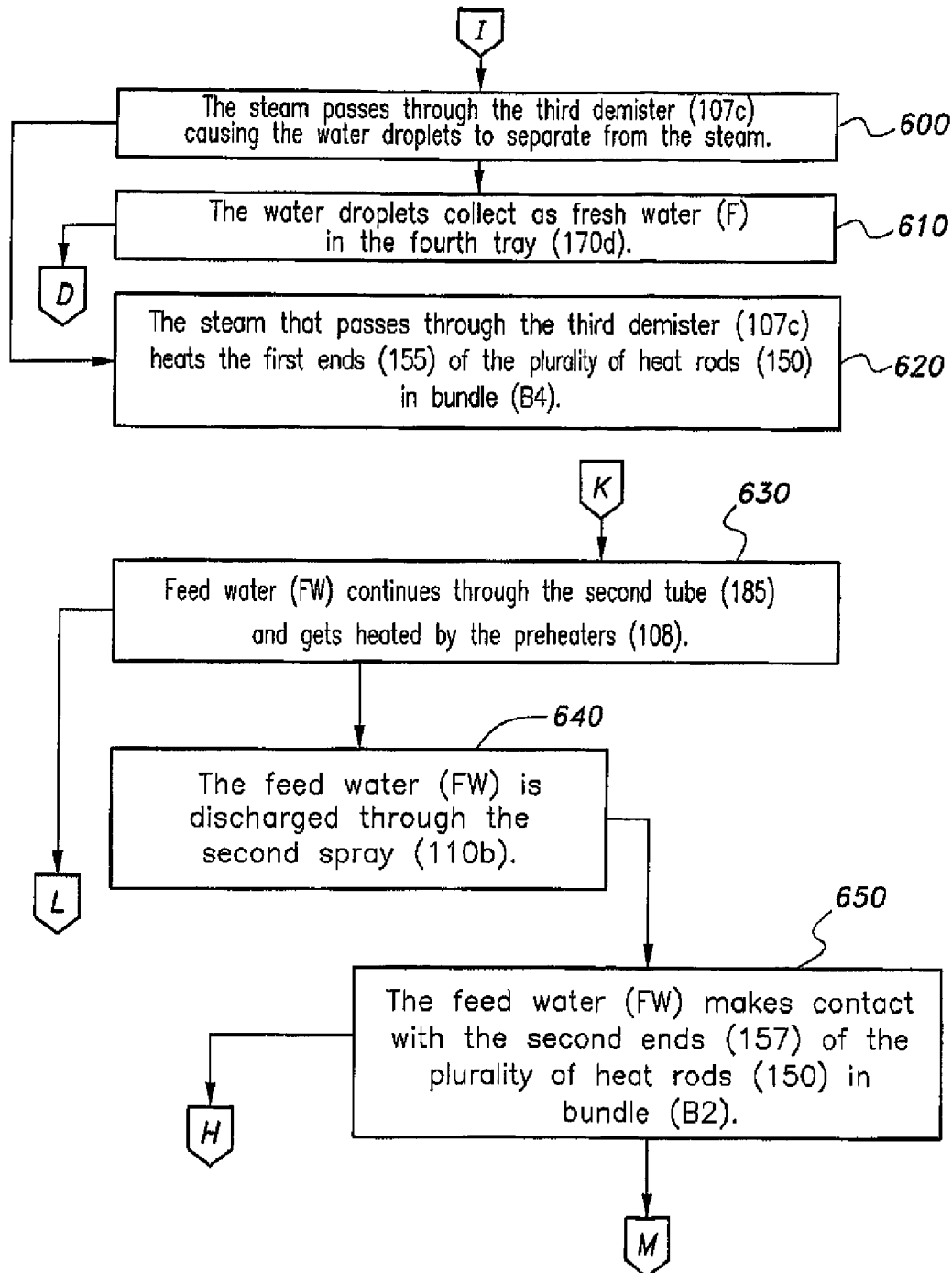
*Fig. 3B*

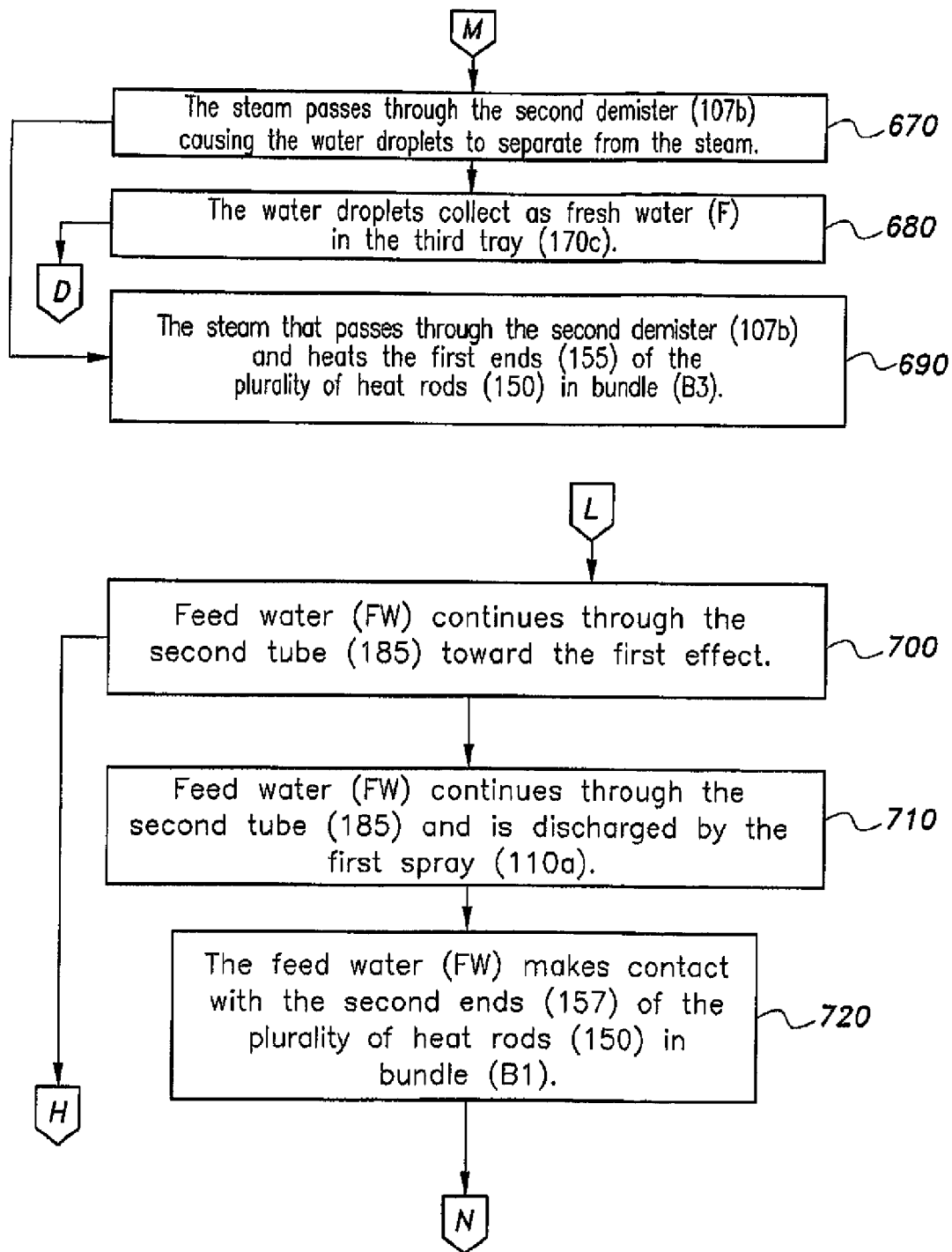
**Fig. 3C**

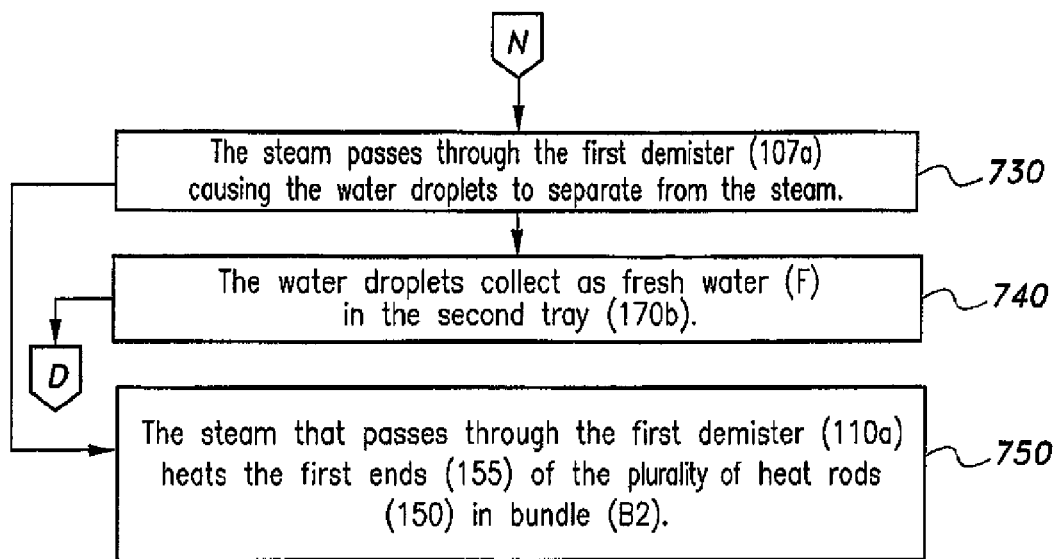
**Fig. 3D**

*Fig. 3E*



**Fig. 3F**

*Fig. 3G*

*Fig. 3H*

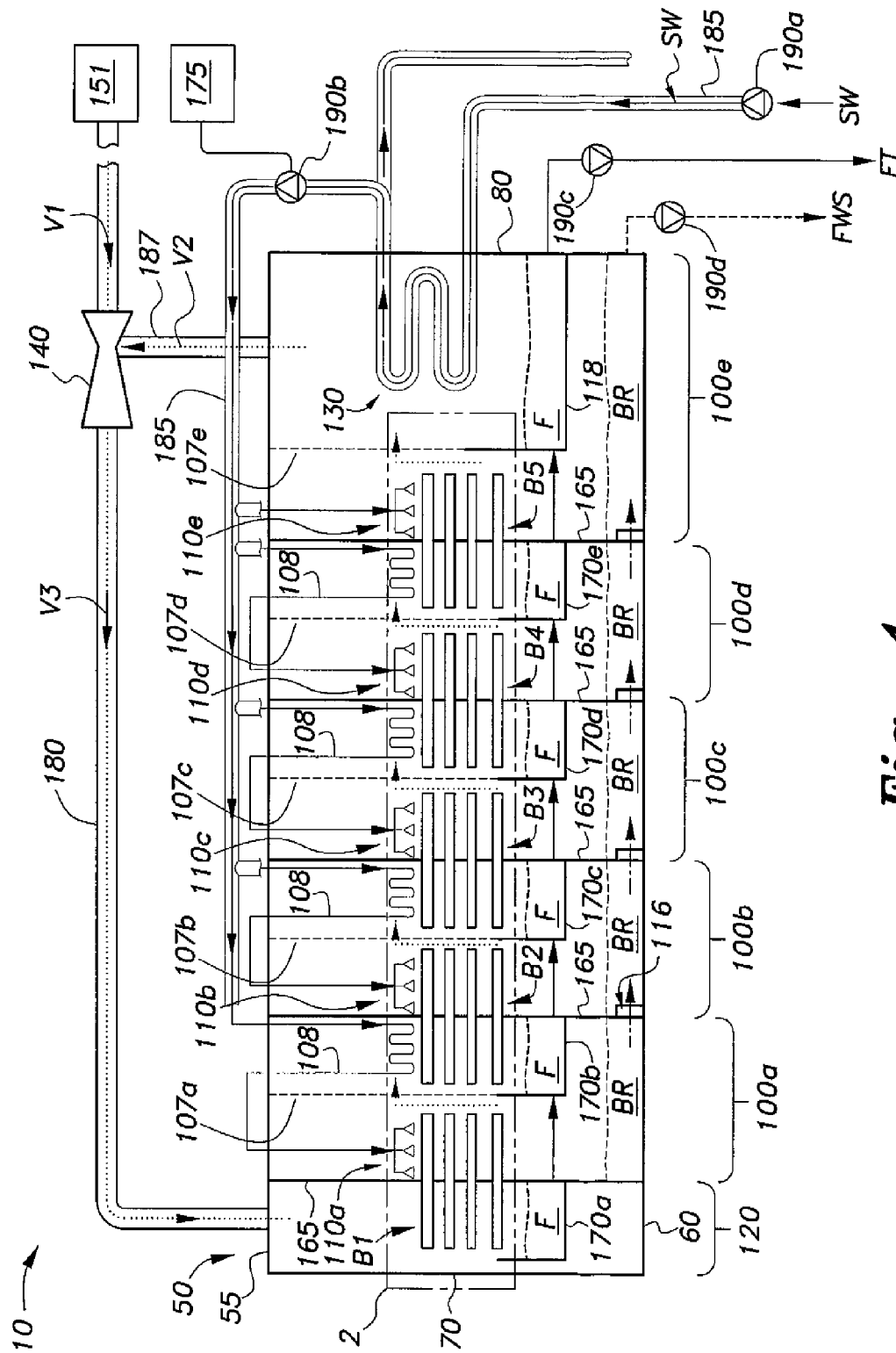


Fig. 4

## MULTI-EFFECTS DESALINATION SYSTEM

## BACKGROUND OF THE INVENTION

## 1. Field of the Invention

The present invention relates generally to desalination systems and, more particularly, to a modified multi-effect distillation thermal vapor compression (MED-TVC) desalination system having a plurality of heat rods.

## 2. Description of the Related Art

Multiple-effect distillation with thermal vapor compression (MED-TVC) is a process used for sea water desalination. Typically, the MED-TVC systems produce desalinated (distillate) water from seawater (salt water), through a multi-stage system which includes horizontal tube bundles at each stage. In each stage, feed water is heated and partially evaporated by the vapor condensing inside the tubes. Saline water evaporates in one stage, and the vapor flows into the tubes of a subsequent stage. Each stage reuses energy from a previous stage. However, the vapor velocity inside the evaporator tubes drops dramatically as it condenses along evaporator tubes. Also, the two phase pressure loss caused by vapor condensing inside the evaporator tubes is high, leading to considerable temperature loss and increase in evaporator heating surface area.

Thus, a multi-effects desalination system solving the aforementioned problems is desired.

## SUMMARY OF THE INVENTION

A multi-effects desalination system includes a housing having a heating box, a plurality of vessels, a plurality of heat rods within each of the vessels, and a condenser unit. Each vessel is separated by a separator wall. Each heat rod extends through one of the separator walls, such that each heat rod has a first end extending into one vessel and a second end extending into an adjacent vessel. The desalination system also includes a plurality of sprayers and a plurality of demisters. Each sprayer is configured to discharge feed water into a respective one of the vessels, e.g., onto the second end of each heat rod in a respective vessel. Each of a plurality of trays, including a first tray, a second tray, a third tray, a fourth tray, and a fifth tray, are positioned underneath the first ends of the heat rods for collecting condensate or fresh water. The condensate collected in one tray can be transferred to the condensate collection tray in an adjacent vessel. Further, the desalination system can also include a thermocompressor unit arranged in communicating relation with a steam source.

These and other features of the present invention will become readily apparent upon further review of the following specification and drawings.

## BRIEF DESCRIPTION OF THE DRAWINGS

FIG. 1 is a schematic diagram of an embodiment of a desalination system having a plurality of effects according to the present invention.

FIG. 2 is a schematic diagram of a portion of the desalination system shown in FIG. 1, showing the ends of the plurality of heat rods for the desalination system according to the present invention.

FIG. 3A a flowchart illustrating a method to desalinate seawater according to the present invention.

FIG. 3B a flowchart illustrating a method to desalinate seawater according to the present invention.

FIG. 3C a flowchart illustrating a method to desalinate seawater according to the present invention.

FIG. 3D a flowchart illustrating a method to desalinate seawater according to the present invention.

FIG. 3E a flowchart illustrating a method to desalinate seawater according to the present invention.

FIG. 3F a flowchart illustrating a method to desalinate seawater according to the present invention.

FIG. 3G a flowchart illustrating a method to desalinate seawater according to the present invention.

FIG. 3H a flowchart illustrating a method to desalinate seawater according to the present invention.

FIG. 4 is a schematic diagram of another embodiment of a desalination system having a plurality of effects according to the present invention.

Similar reference characters denote corresponding features consistently throughout the attached drawings.

## DETAILED DESCRIPTION OF THE PREFERRED EMBODIMENTS

As shown in FIGS. 1 and 2, a multi-effects desalination system 10 includes a housing 50 having a heating box 120, a plurality of vessels, including a first vessel 100a, a second vessel 100b, a third vessel 100c, a fourth vessel 100d, and a fifth vessel 100e, a plurality of heat rods 150 within each of the vessels, and a condenser unit 130. Each vessel 100a-100e is separated by a separator wall 165. By separating each vessel 100a-100e with a separator wall 165, the desalination system 10 can reduce temperature loss and reduce the amount of pressure needed to desalinate feed water FW. Each heat rod 150 extends through one of the separator walls 165. Each heat rod 150 has a first end 155 extending into one vessel and a second end 157 extending into an adjacent vessel (FIG. 2). The desalination system 10 also includes a plurality of sprayers, including a first sprayer 110a, a second sprayer 110b, a third sprayer 110c, a fourth sprayer 110d, and a fifth sprayer 110e. Each sprayer is configured to discharge feed water FW in a respective one of the vessels. For example, each sprayer can discharge feed water FW, such as seawater, onto the second end 157 of each heat rod 150 in a respective vessel. Each of a plurality of trays, including a first tray 170a, a second tray 170b, a third tray 170c, a fourth tray 170d, and a fifth tray 170e, are positioned underneath the first ends 155 of the heat rods 150 for collecting condensate or fresh water (F). The condensate collected in one tray can be transferred to the condensate collection tray in an adjacent vessel through tubing extending between and connecting trays 170a-170e. Further, the desalination system 10 can optionally include a thermocompressor unit 140 arranged in communicating relation with a steam source 151.

The first vessel 100a, the second vessel 100b, the third vessel 100c, the fourth vessel 100d, and the fifth vessel 100e are each configured to accommodate a different effect or stage of desalination occurring in the system 10. The plurality of heat rods 150 can be arranged in any suitable configuration in the vessels. For example, a first bundle of heat rods B1, can include a first plurality of heat rods 150, with first ends 155 disposed in the heat box 120 and second ends 157 disposed in the first vessel 100a. A second bundle of heat rods B2, can include a second plurality of heat rods 150, with first ends 155 disposed in the first vessel 100a and second ends 157 disposed in the second vessel 100b. A third bundle of heat rods B3, can include a third plurality of heat rods 150, with first ends 155 disposed in the second vessel 100b and second ends 157 disposed in the third vessel 100c. A fourth bundle of heat rods B4, can include a fourth plurality of heat rods 150, with first ends 155 disposed in the third vessel 100c and second ends disposed in the fourth vessel 100d. A fifth bundle of heat

rods B5, can include a fifth plurality of heat rods 150, with first ends 155 disposed in the fourth vessel 100d and second ends in the fifth vessel 100e.

The desalination system 10 further includes a plurality of demisters including a first demister 107a, second demister 107b, a third demister 107c, a fourth demister 107d, and a fifth demister 107e. The first demister 107a extends between the first bundle of heat rods B1 and the second bundle of heat rods B2. The second demister 107b extends between the second bundle of heat rods B2 and the third bundle of heat rods B3. The third demister 107c extends between the third bundle of heat rods B3 and the fourth bundle of heat rods B4. The fourth demister 107d extends between the fourth bundle of heat rods B4 and the fifth bundle of heat rods B5. A plurality of pumps 190a-190d are provided, including a first pump 190a configured for pumping feed water FW upward through a second tube 185 from a feed water source FWS, such as the ocean, a second pump 190b configured to pump the feed water FW through the second tube 185 toward the first vessel 100a, a third pump 190c configured to pump fresh water F from a fresh water tray 118 into a fresh water tank FT, and a fourth pump 190d configured for pumping brine water BR into the feed water source FWS.

The desalination system 10 can also include a power source 175, such as solar panels or wind turbines, coupled to the first pump 190a, the second pump 190b, the third pump 190c, and/or the fourth pump 190d to power the desalination system 10. The thermocompressor unit 140 receives a first vapor V1 from the steam source 151. The steam source can be a conventional boiler or any type of suitable steam boiler operating from a renewable energy source such as solar, geothermal, waste heat, or a biomass energy source. The first vapor V1 is used to extract a second vapor V2 from one or more vessels 100a-100e through a third tube 187 to create a total or combination vapor V3, which is fed into the heating box 120 through a first tube 180.

The first ends 155 of the plurality of heat rods 150 in bundle B1 are heated in the heating box 120. Heat is transferred from the first ends 155 to the second ends 157 of the heat rods 150 in bundle B1. The first spray 110a releases feed water FW onto the second ends 157 of the plurality of heat rods 150 in the first vessel 100a to generate steam. In other words, heat transferred from the first ends 155 to the second ends 157 partially evaporates the spray of water falling from the sprayer 110a. The vapor or steam produced in the first vessel 100a flows through the demister 107a. The demister 107a separates water droplets from the steam, which are collected in the second tray 170b. The remaining steam heats the first ends 155 of the second bundle B2 of heat rods 150. In this manner, the first ends 155 of the heat rods 150 of the second bundle B2 are heated. The steam flowing through the demister 107a also provides heat to the preheater tubes 108 in the first vessel 100a. The preheater tubes 108 can heat water that is fed into the first vessel 100a. Vapor is produced in the remaining vessels 100b-100d and transferred to an adjacent vessel in a similar fashion. The vapor formed in the last vessel 100e is forwarded to the condenser unit 130 through the demister 107e. The condenser unit 130 condenses the generated steam into fresh water F to be pumped into the fresh water tank FT at atmospheric pressure. As condensation occurs on outer surfaces of the pipes or tubes and not inner surfaces, pressure drop inside the tube and associated temperature loss are avoided.

It is contemplated that there can be "n" effects (stages) and "n" corresponding vessels in the desalination system 10, whereas "n" can be either greater than or less than five. It is to be noted that each of the plurality of (desirably five) effects

(stages) occurs in a separate vessel. For example, the first effect can take place in the first vessel 100a, the second effect can take place in the second vessel 100b, the third effect can take place in the third vessel 100c, the fourth effect can take place in the fourth vessel 100d, and the fifth effect can take place in the fifth or last vessel 100e. Further, each effect (stage) can operate at a higher boiling temperature and pressure than the subsequent effect (stage).

The housing 50 can have a top portion 55, a bottom portion 60, a first side 70, and a second side 80. The housing 50 can be made from any suitable material, such as steel, configured to retain heat and collect the brine water BR. The plurality of vessels, such as the first vessel 100a, the second vessel 100b, the third vessel 100c, the fourth vessel 100d, and the fifth vessel 100e can have any suitable shape, such as a generally rectangular shape, and can be arranged in a horizontal configuration, as illustrated in FIG. 1. The separator wall 165 separating each vessel can include an opening 116, to allow the brine BR to flow and flash through the successive vessels, e.g., from the first vessel 100a through the second vessel 100b, the third vessel 100c, the fourth vessel 100d, and the fifth vessel 100e, so that the brine BR can be discharged into the feed water source FWS. Tubing connecting the first through fifth trays 170a-170e and the fresh water tray 118 can also extend through the separator walls 165.

The heating box 120 can be made from any suitable material, such as steel. The heating box 120 can have any suitable shape, such as a generally rectangular shape. The heating box 120 can house the first ends 155 of the plurality of heat rods 150 in bundle B1. Further, the condenser unit 130, configured to cool the steam received from the fifth vessel 100e, can be positioned in the fifth vessel 100e. The fifth vessel 100e can house the second ends 157 of the plurality of heat rods 150 in bundle B5, as illustrated in FIG. 1.

Each of the plurality of heat rods 150 can be formed from steel, or any suitable material that can absorb large amounts of heat, such as the heat from the vapor V3 emitted by the thermocompressor 140, and can have any suitable length and width sufficient to absorb the maximum amount of heat emitted by the thermocompressor unit 140. It is to be noted that the plurality of heating rods 150 can include a plurality of heating rods, heating pipes, or heat pipe systems. Each of the bundles B1, B2, B3, B4, and B5 can extend through a respective one of the separator walls 165, so that the heat received by the first ends 155 in one vessel can be transferred to the second ends 157 of the plurality of heat rods 150 in an adjacent vessel.

The first ends 155 of each heat rod 150 in bundle B1 can be positioned in the heating box 120 so as to receive the heat from the steam introduced by the thermocompressor unit 140 through the first tube 180. The first ends 155 transfer the heat to the corresponding second end 157 of each heat rod 150 in bundle B1 positioned in the first vessel 100a. When the second ends 157 receive the feed water FW from the first spray 110a, steam is created. The steam passes through the demister 107a and heats the first ends 155 of each heat rod 150 in bundle B2 that are housed in the first vessel 100a. The second ends 157 of the plurality of heat rods 150 in bundle B1 are separated from the first ends 155 of the plurality of heat rods 150 in bundle B2 by the first demister 107a.

The first ends 155 of each heat rod 150 in bundle B2 can be housed in the first vessel 100a and the corresponding second ends 157 of each heat rod 150 in bundle B2 can be housed in the second vessel 100b. The first ends 155 of each heat rod 150 in bundle B3 can be housed in the second vessel 100b and the corresponding second ends 157 of each heat rod 150 in bundle B3 can be housed in the third vessel 100c. The second ends 157 of the plurality of heat rods 150 in bundle B2 can be

5

separated from the first ends **155** of the plurality of heat rods **150** in bundle **B3** by the second demister **107b**, as illustrated in FIG. 1. The number of effects will determine the number of bundles of heat rods in the desalination system **10**, as well as the corresponding number of demisters.

Each sprayer **110a-110e** can be positioned within a respective vessel **100a-100e** over the second ends **157** of the plurality of heat rods **150** in a respective bundle **B1, B2, B3, B4, and B5**. Each of the plurality of sprayers **110a-110e** can be arranged in communicating relation with the second tube **185**, thereby receiving the feed water FW from the feed water source FWS. The sprayers, such as sprayers **100a-110c**, can be any suitable type of sprayer, as is well known in the art, configured to discharge the feed water FW received from the feed water source FWS onto the second ends **155** of the plurality of heat rods **150** housed within each of the plurality of vessels.

It is to be noted that the feed water FW can be fed through the second tube **185** and into the plurality of sprayers by any suitable configuration. In one embodiment, for example, the sprayers **110a-110e** can be arranged in series, as illustrated in FIG. 1, in which the feed water FW passes through each preheater tube **108** and corresponding sprayer, such as sprayers **110a-110e**, successively. In another embodiment, the sprayers **110a-110e** can be arranged in parallel, as illustrated in FIG. 4, in which the feed water FW passes through each preheater tube **108** and each corresponding sprayer, such as sprayers **110a-110e**, at the same time.

Referring to FIGS. 3A-3H, a process by which feed water FW, such as seawater, is desalinated using the desalination system **10** is described. To start (Step **300**) the desalination system **10**, vapor **V1** is pushed through the thermocompressor unit **140** and through the first tube **180** into the heating box **120** (Step **310**). The vapor then comes in contact with the first ends **155** of the plurality of heat rods **150** in bundle **B1** and heats the first ends **155** of the plurality of heat rods **150** in bundle **B1** (Step **320**). Any condensation that results from the heating of the first ends **155** of the plurality of heat rods **150** in bundle **B1**, as described in Step **320**, can be collected as fresh water F by the first tray **170a** and throttled to the second tray **170b**. Feed water FW is drawn upward by the first pump **190** through the second tube **185** and through the condenser unit **130** (Step **330**). After the feed water FW passes through the condenser unit **130**, some of the feed water FW is pumped through the second tube **185** towards the first vessel **100a** (Step **360**) and a remaining portion of the feed water FW is released back into the feed water source FWS (Step **340**), where the feed water FW can get drawn upward again through the second tube **185** to the condenser unit **130** (Step **360**).

The feed water FW in the second tube **185** is discharged through the fifth spray **110e** onto the second end **157** of the plurality of heat rods **150** in bundle **B5** (Step **370**). The feed water FW makes contact with the second ends **157** of the plurality of heat rods **150** in bundle **B5** (Step **380**), and a portion of the feed water FW collects at the bottom of the fifth vessel **100e** (Step **390**) as brine BR. The brine BR is then discharged into the feed water source FWS (Step **400**).

Once the feed water FW makes contact with the second ends **157** of the plurality of heat rods **150** in bundle **B5** as described in Step **380**, a portion of the feed water FW evaporates and turns into steam (Step **410**). The steam that is produced passes through the fifth demister **107e** that separates the second ends **157** of the plurality of heat rods **150** in bundle **B5** from the condenser unit **130**, thereby causing water droplets to separate from the steam (Step **420**). The water droplets then collect at the bottom of the fifth vessel **100e** as fresh water F (Step **430**).

6

Some of the steam in the fifth vessel **100e** is drawn up as vapor **V2** through the third tube **187** into the thermocompressor unit **140** to mix with the vapor **V1** from the steam source **151** (Step **450**) and the process continues as described in Step **310**. The remaining steam in the fifth vessel **100e** contacts the condenser unit **130**, condenses on the tube bundle of the condenser unit **130**, and is thereby converted into fresh water F (Step **460**). The fresh water F collects in the fresh water tray **118** (Step **470**). The fresh water F is then discharged into the fresh water tank FT (Step **480**) and the process ends (Step **490**).

A portion of the feed water FW in tube **185** is discharged through the sprayer **110e** as described in Step **370**, and a remaining portion of the feed water FW continues through the second tube **185** and is progressively fed into each of the adjacent vessels **100a-100d** (Step **500**). The feed water FW is preheated by the preheater tubes **108** of the fourth vessel **100d** and is discharged through the fourth sprayer **110d**, contacting the second ends **157** of the plurality of heat rods **150** in bundle **B4**. A portion of the feed water evaporates (Step **520**) or transforms to steam which passes through the fourth demister **107d** causing water droplets to separate from at least some of the steam (Step **530**). After the water droplets separate from the steam, the water droplets collect in the tray **170e** as fresh water (Step **540**). The steam remaining in the fourth vessel **100d** heats the first ends **155** of each of the plurality of heat rods **150** in bundle **B5** (Step **550**). The heat transfers to the second ends **157** of the plurality of heat rods **150** in the fifth bundle **B5** (Step **560**).

A portion of the feedwater in the second tube **185** is preheated by the preheater tubes **108** of the fourth vessel **100d** and a remaining portion continues into the third vessel **100c**. In the third vessel **100c**, the feed water FW is preheated by the preheater tubes **108** and discharged through the third spray **110c** (Step **580**). When the feed water FW is discharged by the third spray **110c**, it makes contact with the second ends **157** of the plurality of heat rods **150** in bundle **B3** and a portion of the feed water evaporates and transforms into steam (Step **590**). The steam passes through the third demister **107c** causing water droplets to separate from at least some of the steam (Step **600**). After the water droplets separate from the steam, the water droplets collect in tray **170d** as fresh water F (Step **610**). The steam remaining in the third vessel **100c** heats the first ends **155** of the plurality of heat rods **150** in bundle **B4** (Step **620**).

The remaining feed water FW flowing through the second tube **185** continues through the second tube **185** and is preheated by the preheater tubes **108** in the second effect (Step **630**). The feed water FW is discharged through the second spray **110b** (Step **640**) and makes contact with the second ends **157** of the plurality of heat rods **150** in bundle **B2** (Step **650**). The feed water FW evaporates and converts into steam upon contacting the second ends **157** of the plurality of heat rods **150** in bundle **B2**. The steam passes through the second demister **107b** causing the water droplets to separate from the steam (Step **670**). After the water droplets separate from the steam, the water droplets collect in the third tray **170c** as fresh water F (Step **680**). The steam that passes through the second demister **107b** heats the first ends **155** of the plurality of heat rods **150** in bundle **B3** (Step **690**).

The remaining feed water FW flowing through the second tube **185** is preheated by preheaters **108** in the first vessel **100a** as it is pumped into the first effect (Step **700**). The feed water FW continues through the second tube **185** and is discharged by the first spray **110a** (Step **710**). Once the feed water FW is discharged by the first spray **110a**, the feed water FW makes contact with the second ends **157** of the plurality of

7

heat rods **150** in bundle B1 (Step **720**). The spray evaporates upon contacting the second ends **157** of the plurality of heat rods **150** in bundle B1. The steam passes through the first demister **107a** causing the water droplets to separate from the steam (Step **730**). After the water droplets separate from the steam, the water droplets collect in tray **170b** as fresh water F (Step **740**). The steam that passes through the first demister **107a** heats the first ends **155** of the plurality of heat rods **150** in bundle B2 (Step **750**).

It is to be understood that the present invention is not limited to the embodiments described above, but encompasses any and all embodiments within the scope of the following claims.

We claim:

1. A desalination system, comprising:

a housing including a heating box, a condenser unit, a plurality of vessels, and a plurality of separator walls, each separator wall between adjacent vessels;

a first tubing;

a thermocompressor unit operatively connected to the heating box by the first tubing;

a plurality of demisters, each of the plurality of demisters being substantially vertically disposed in a respective one of the plurality of vessels;

a plurality of heat rods disposed horizontally in each vessel, each heat rod having a first end and a second end, the first end extending into one of the plurality of vessels and the second end extending into an adjacent one of the plurality of vessels;

wherein each of the plurality of heat rods extend through the separator wall between adjacent vessels;

a plurality of sprayers, each of the plurality of sprayers positioned in a respective one of the plurality of vessels;

a plurality of preheaters, each of the plurality of preheaters positioned in a respective one of the plurality of vessels;

at least one condensate tray disposed in each one of the plurality of vessels for receiving condensate;

a second tubing extending between a feed water source, the plurality of preheaters, and the plurality of sprayers; and a plurality of pumps, each pump designed and configured for selectively moving fluid;

wherein the fluid is selectively moved through the second tubing, and from the at least one condensate tray.

2. The desalination system according to claim 1, further comprising a steam source.

3. The desalination system according to claim 1, further comprising a fresh water tray in communication with each one of the at least one condensate tray in each of the plurality of vessels for receiving fresh water.

4. A desalination system, comprising:

a heating box;

a condenser unit;

a plurality of vessels disposed between the heating box and the condenser unit wherein each vessel of the plurality of vessels consisting of:

a preheater;

a sprayer;

at least one condensate tray for receiving condensate;

a demister vertically disposed therein for separating water droplets from water vapor; and

a floor for collecting brine;

a plurality separator walls;

wherein the plurality of separator walls operatively disposed between the heating box, the plurality of vessels, and the condenser unit;

8

each one the separator walls between adjacent vessels and the condenser unit including an opening configured to allow brine to flow therethrough;

a plurality of heat rod groups, each heat rod group extending horizontally through one of a corresponding separator wall;

wherein a first end of each heat rod in each of the heat rod groups being disposed on one side of the separator wall, and a second end of each heat rod in each of the heat rod groups being disposed on an opposite side of the separator wall, such that each vessel has the first end of one of the heat rod groups and the second end of another one of the heat rod groups; and

wherein the heating box has the first end of the first heat rod group, and the condenser unit has the second end of the ultimate heat rod group;

whereby the preheater of each vessel receives heat the first end of the heat rod group and the sprayer of each vessel deposit feedwater onto the second end of the heat rod group, the second end of the heat rod group condensing freshwater into the condensate tray;

a fresh water tray in communication with each condensate tray of each vessel for receiving fresh water;

a first tubing;

a thermocompressor unit;

a steam source;

wherein the first tubing coupling the steam source to the thermocompressor, and the thermocompressor to the heating box;

a second tubing serially coupling the plurality of sprayers and preheaters of each vessel to a feedwater source;

a first pump for pumping feed water into the condenser unit;

a second pump for pumping feed water from the condenser unit into the second tubing;

a third pump for pumping freshwater from the freshwater tray; and

at least one other pump, the at least one other pump for pumping brine to the feedwater source.

5. A method for desalinating seawater, comprising the steps of:

providing a housing successively including a heating box, a plurality of vessels, and a condenser unit: a separator wall disposed between each of adjacent ones of the heating box, the plurality of vessels, and the condenser unit, each one of the plurality of vessels including a demister positioned vertically therein, a thermocompressor unit being connected to the heating box by a first tubing, a plurality of heat rods disposed horizontally between each of the adjacent heating box, plurality of vessels, and condenser unit, each heat rod having a first end on one side of one of the separator walls and a second end on the opposite side of the separator wall, a plurality of preheaters, each of the plurality of preheaters in a respective one of the plurality of vessels, a plurality of sprayers, each of the plurality of sprayers disposed in a respective one of the plurality of vessels, a second tubing extending between a feed water source, the plurality of preheaters, and the plurality of sprayers, and a plurality of pumps for selectively pumping feedwater, brine, and freshwater through the housing;

introducing a first vapor from a steam source into the first tubing and through the thermocompressor unit;

producing a second vapor in at least one of the plurality of vessels;

combining the first vapor and the second vapor to form a third vapor;



directing the third vapor into the heating box;  
heating the first ends of the plurality of heat rods in the  
heating box;  
discharging feed water from the feed water source onto the  
second ends of the plurality of heat rods in a first vessel 5  
of the plurality of vessels to create steam;  
preheating the feed water prior to discharging the feed  
water onto the second ends of the plurality of heat rods;  
separating water droplets from the steam produced in the  
first vessel using the demister in the first vessel; 10  
heating the first ends of the plurality of heat rods in the first  
vessel by the steam;  
discharging feed water from the feed water source onto the  
second ends of the plurality of heat rods in a second  
vessel of the plurality of vessels to create steam; 15  
preheating the feed water prior to discharging the feed  
water onto the second ends of the plurality of heat rods;  
separating water droplets from the steam produced in the  
second vessel using the demister in the second vessel;  
condensing the steam produced in the second vessel of the 20  
plurality of vessels on the condenser unit; and  
collecting fresh water.

6. The method for desalinating seawater according to claim  
5, wherein feed water is discharged from the feed water  
source onto the second ends of the plurality of heat rods in the 25  
first vessel before feed water is discharged from the feed  
water source onto the second ends of the plurality of heat rods  
in the second vessel.

7. The method for desalinating seawater according to claim  
5, wherein feed water is simultaneously discharged from the 30  
feed water source onto the second ends of the plurality of heat  
rods in the first vessel and the second vessel.

\* \* \* \* \*